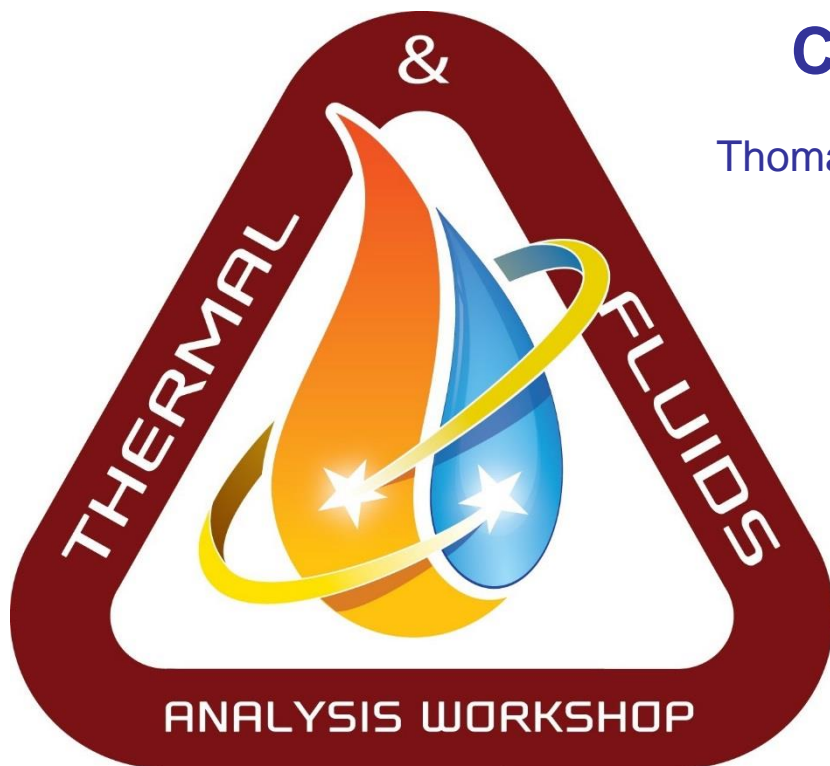




## Acoustic Actuation of Vapor-Liquid Interfaces in Boiling and Condensation Processes

Thomas R. Boziuk, Marc K. Smith, and Ari Glezer  
School of Mechanical Engineering  
Georgia Institute of Technology  
Atlanta, GA

Presented By  
**Marc K. Smith**



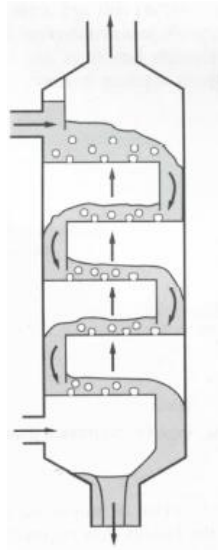
**TFAWS**  
MSFC • 2017

Thermal & Fluids Analysis Workshop  
TFAWS 2017  
August 21-25, 2017  
NASA Marshall Space Flight Center  
Huntsville, AL

# Two-Phase Power Dissipation Applications



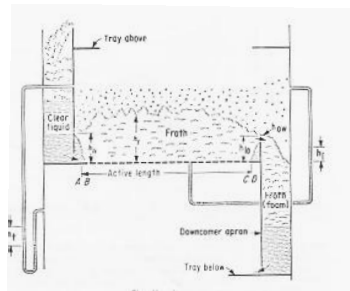
Server Farm



Insulated-Gate Bipolar Transistor



Radar



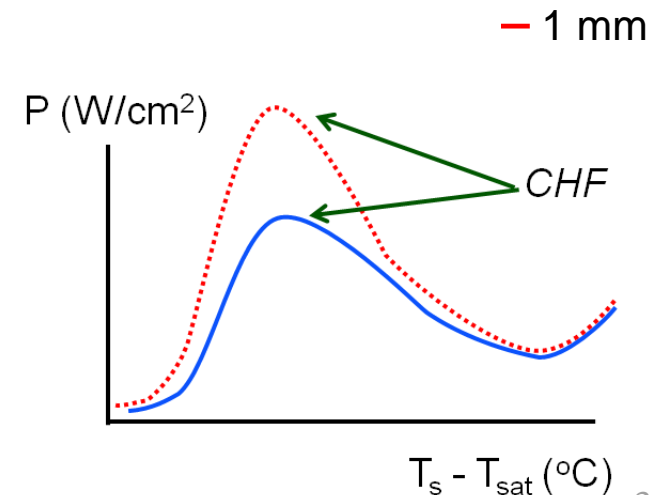
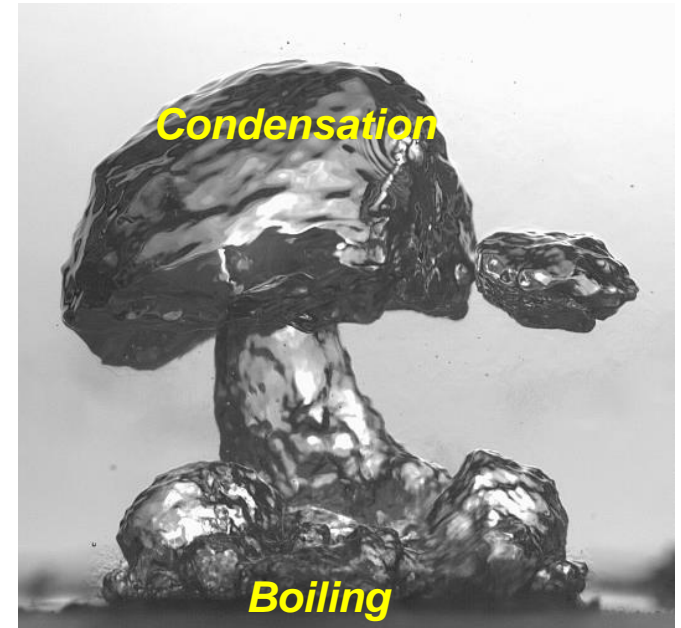
Chemical / Process Engineering



Electric Vehicle Drivetrains

# Control of Phase Change Heat Transfer

- Boiling heat transfer for high-power, dense electronic systems
- Heat transfer is limited by two primary processes
  - » Vapor formation and removal rates (critical heat flux)
  - » Condensation rate
- Boiling and condensation present different design challenges
  - » Boiling: increase CHF, decrease surface superheat
  - » Condensation: enhance in bulk fluid for efficient thermal packaging
- Acoustic control of 2-phase boiling processes
  - » *At heater surface* control of vapor growth, spreading, and advection
    - Surface force engendered by high-frequency ultrasound
    - Used in conjunction with complex boiling geometries
  - » *In bulk fluid* control of condensation
    - Acoustic actuation couples to surface Faraday waves **or** via radiation pressure force and droplet ejection
    - Pool boiling and nozzle condensation geometries

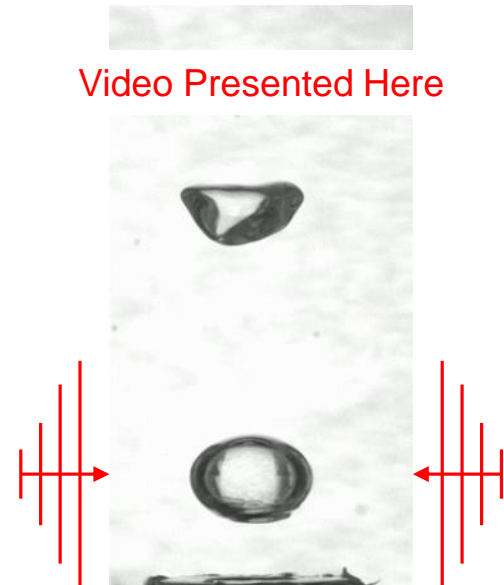


# Acoustic Actuation of Liquid/Gas Interface

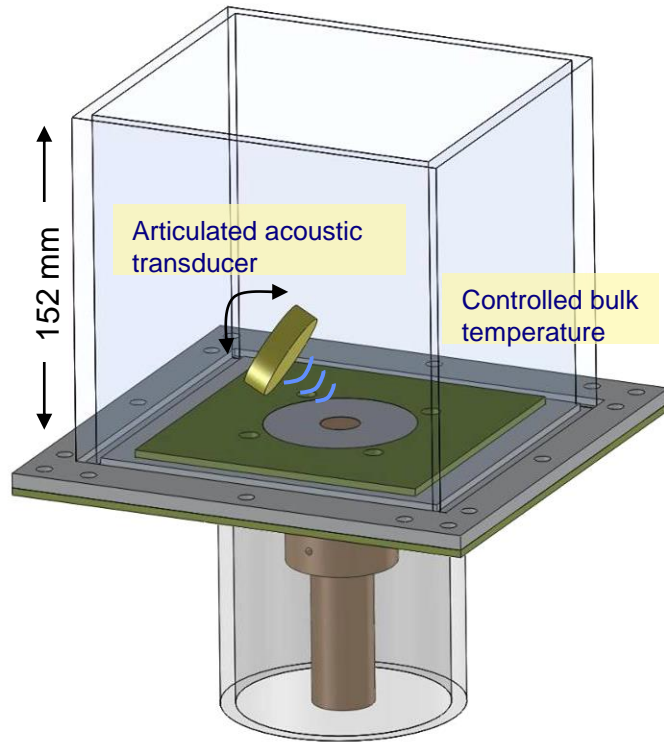
- Interfacial coupling varies substantially with actuation wavelength
- Ultrasonic [O(1 MHz)] liquid/gas interfacial actuation
  - » **Short actuation wavelength** [O(1 mm)]
    - Exploits acoustic surface force to effect interfacial deformations and injection of a liquid jet and droplets
  - »  $\lambda_{\text{acoust}} = 0.9 \text{ mm}$ ;  $D_{\text{res}} = 2 \text{ }\mu\text{m}$ ;  $\lambda_{\text{capillary}} = \text{O}(\mu\text{m})$
  - » Impedance mismatch
    - $Z_{\text{vapor}}/Z_{\text{water}} = 1.8 \times 10^{-4}$
  - » High acoustic absorption coefficient
    - $\alpha_{\text{H}_2\text{O vapor}} \approx 1,000 \alpha_{\text{H}_2\text{O liquid}}$
  - » Amplitude =  $6.82 \cdot 10^3 \text{ kPa}$  peak-to-peak
  - » Forcing affects vapor bubbles larger than  $D_{\text{res}}$
- O(1 kHz) liquid/gas interfacial actuation
  - » **Long actuation wavelength** [O(1 m)]
    - Much larger than the characteristic length scale of the vapor bubbles [O(5-10 mm)]
    - Forces capillary surface waves to enhance mixing of the interfacial thermal boundary layer
  - »  $\lambda_{\text{acoust}} = 1.5 \text{ m}$ ;  $D_{\text{res}} = 5.5 \text{ mm}$ ;  $\lambda_{\text{capillary}} = \text{O}(\text{mm})$ 
    - Significant disturbances
  - » Amplitude = 5 kPa peak-to-peak
  - » Bjerknes body forces affect bubble's path



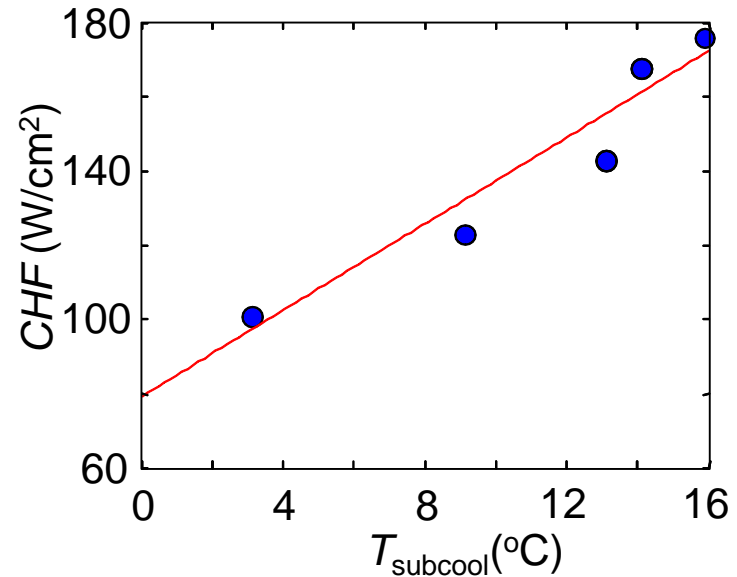
Video Presented Here



# Acoustically Controlled Boiling: Experimental Setup



Variation of Critical Heat Flux with Bulk Temperature

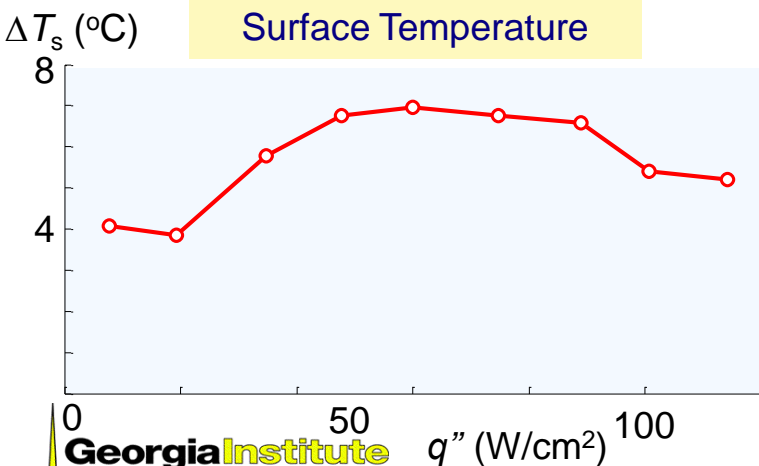
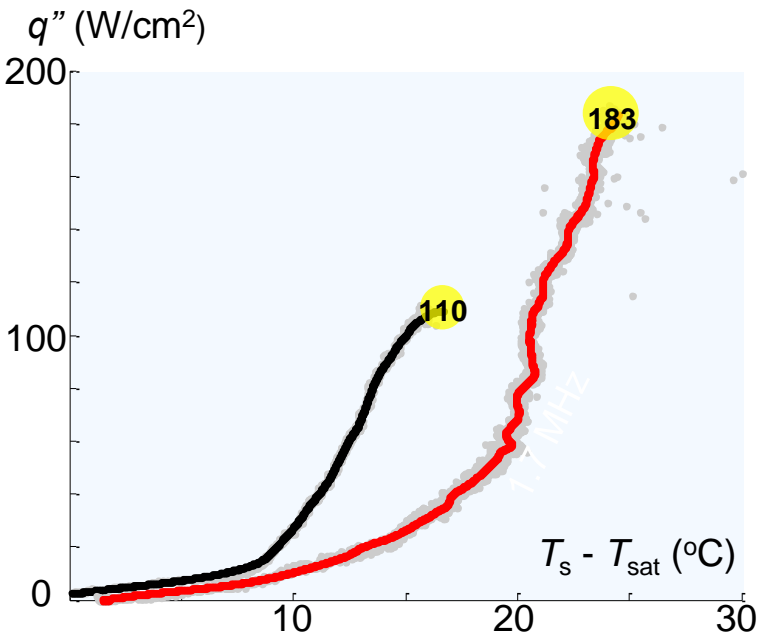


- Heated surface design
  - » Cartridge heater and thermocouples
  - » Exchangeable heater surfaces
    - Plain
    - Plain, instrumented with surface-soldered thermocouples
    - Microchannel grid

Distilled water  
1 atm  
93°C bulk temperature



# Ultrasonic Control of Vapor at Surface

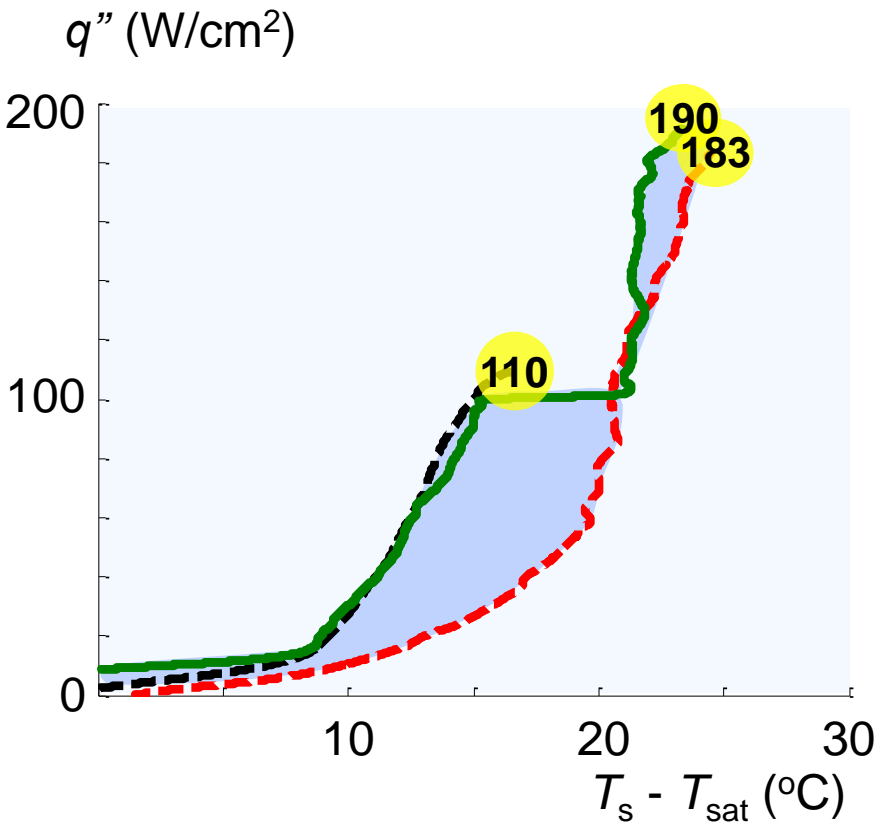


Vapor removal at surface  
50 W/cm<sup>2</sup>

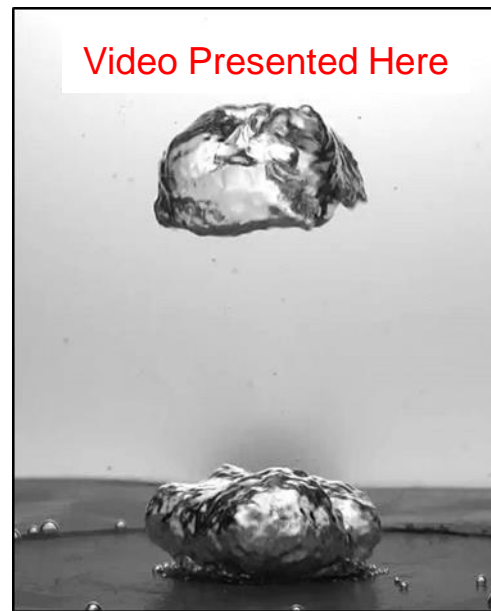
## High-frequency acoustic actuation

- » Increases surface temperature (7 °C)
  - Detaches small scale vapor bubbles
  - Suppresses vaporization process at most nucleation sites
- » Increases CHF by 65%
  - Agreement with wire experiments of Isakoff (1956)

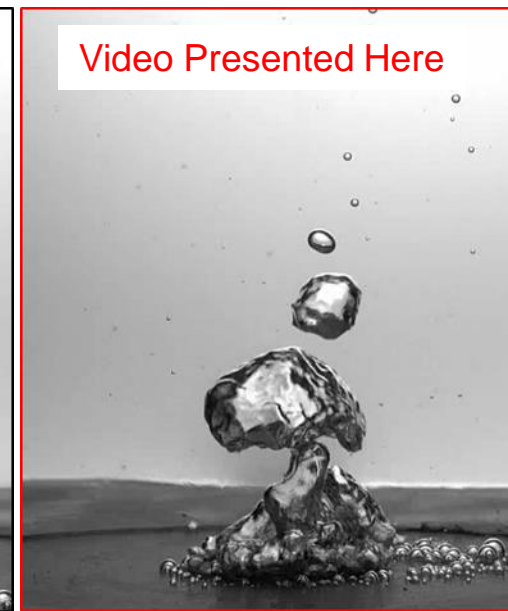
# Ultrasonic Control of the Boiling Curve



No Actuation



Acoustic Actuation  
(1.7 MHz)

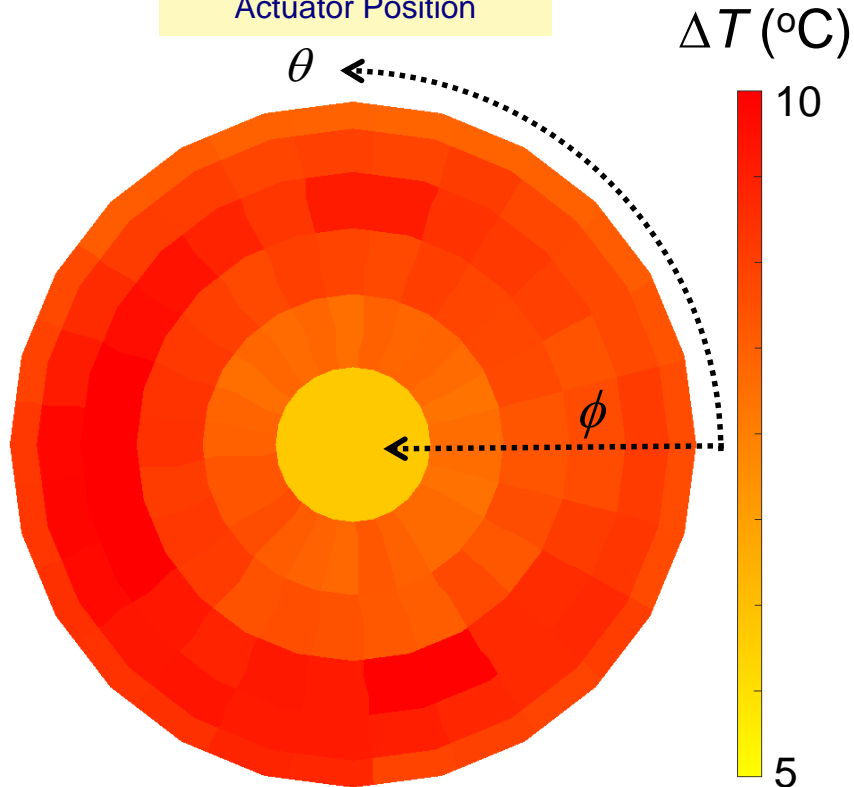


$q'' = 100$   
W/cm<sup>2</sup>

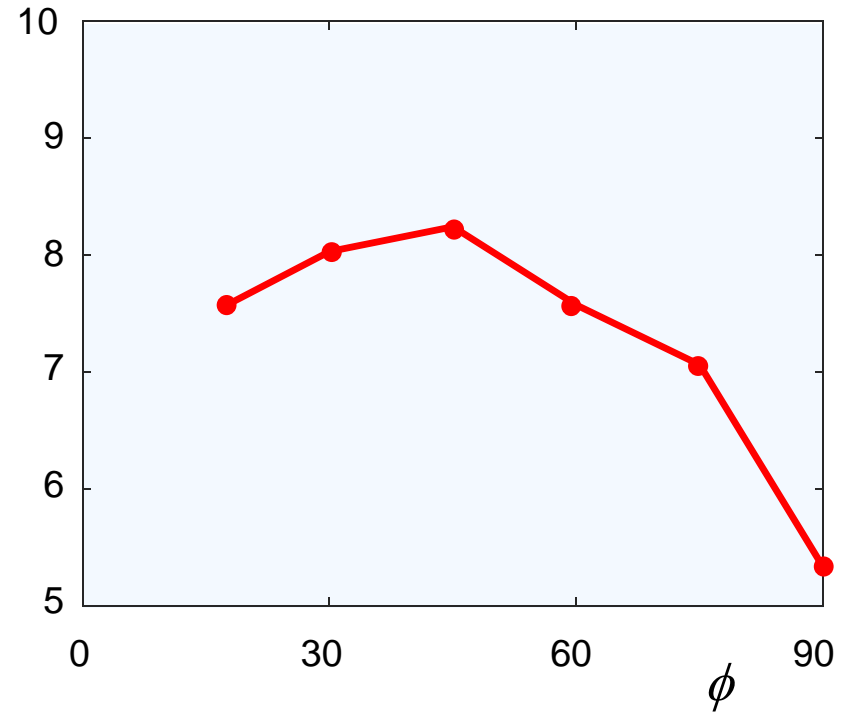
— 1 mm

# Effect of Actuator Incidence Angle

$\Delta T$  as function of  
Actuator Position



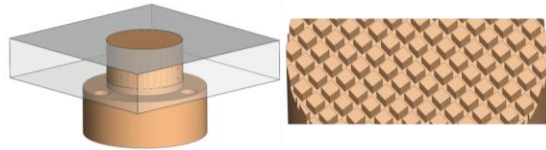
$\overline{\Delta T}$



$$q''_{\text{base}} = 100 \text{ W/cm}^2, T_{\text{base}} = 110^\circ\text{C}, T_{\text{bulk}} = 93^\circ\text{C}$$



# microChannel Design: More than Surface Area

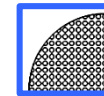
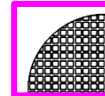
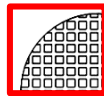
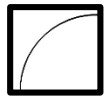


Smooth

microChannels

Dimpled

approx. same wetted area



1000

400

200

$q''$  (W/cm<sup>2</sup>)

400

Normalized by projected area

200

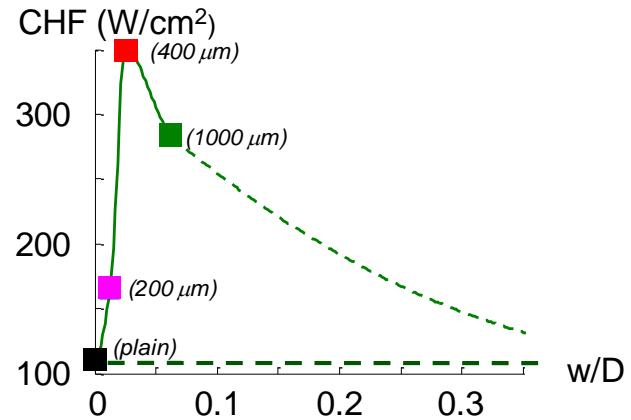
0

10

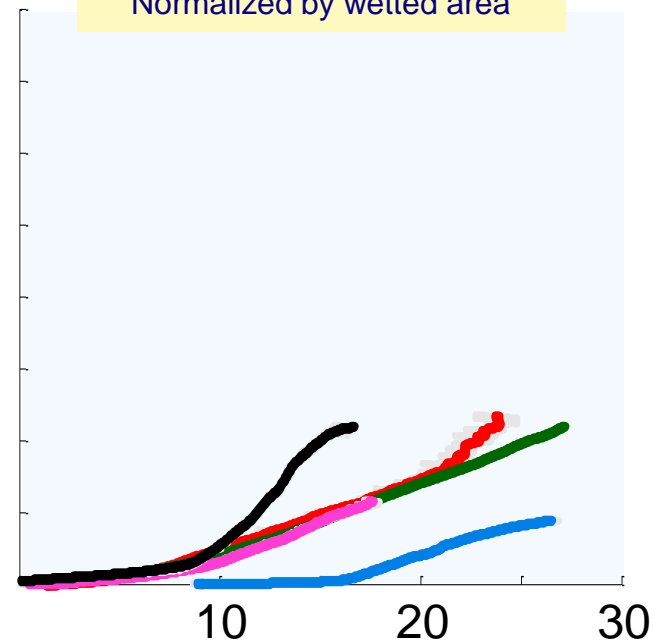
20

30

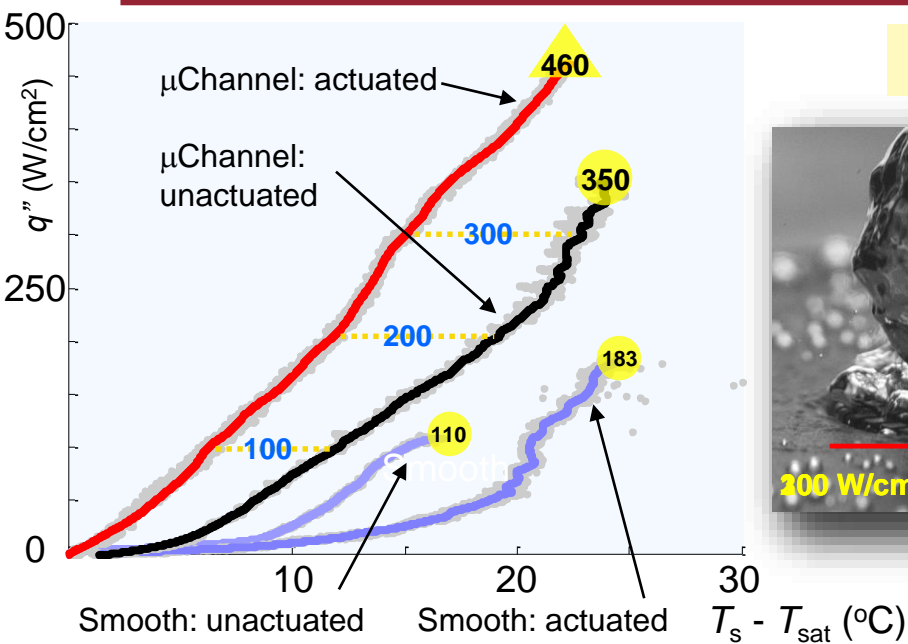
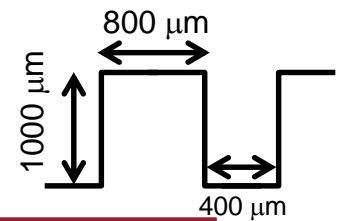
$T_s - T_{\text{sat}}$  (°C)



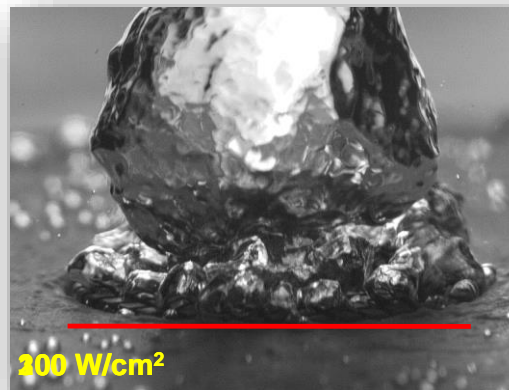
Normalized by wetted area



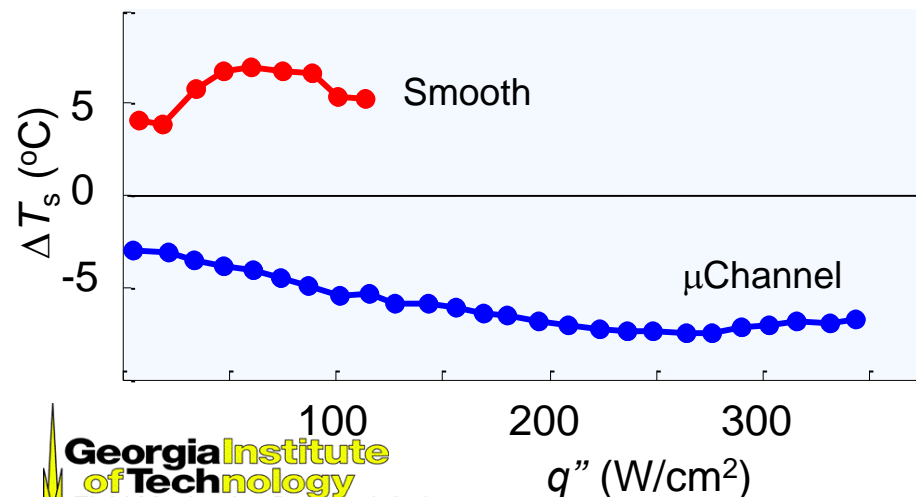
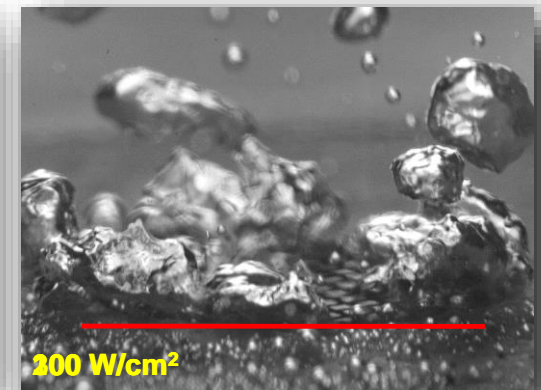
# Surface $\mu$ Channels with Ultrasonic Actuation



$\mu$ Channel



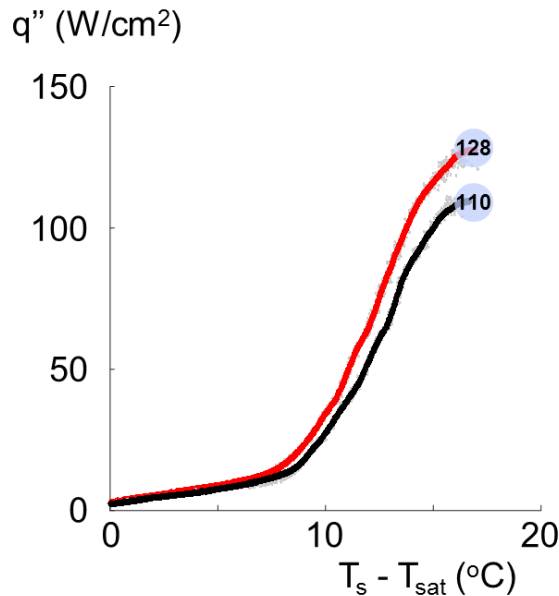
Actuated (1.7 MHz)



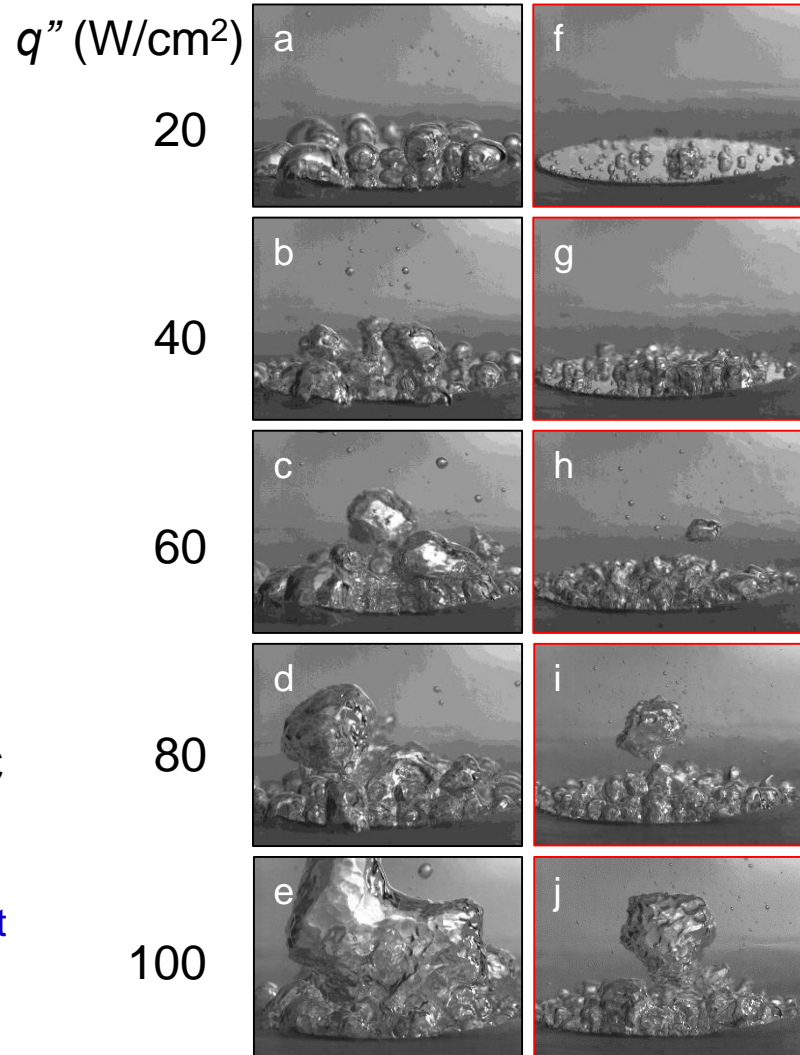
## Small-scale acoustic actuation within $\mu$ Channels

- » Decreases surface temperature ( $\sim 7$  °C).
- » Increased power dissipation  $\Delta P \approx 200$  W/cm<sup>2</sup> at  $T_s - T_{sat} = 17$  °C
- » Increases CHF by 31%
- » Decreases surface temperature fluctuations.
- » Increase CHF by 318% relative to smooth, unactuated case

# O(1 kHz) Acoustic Enhancement of Boiling

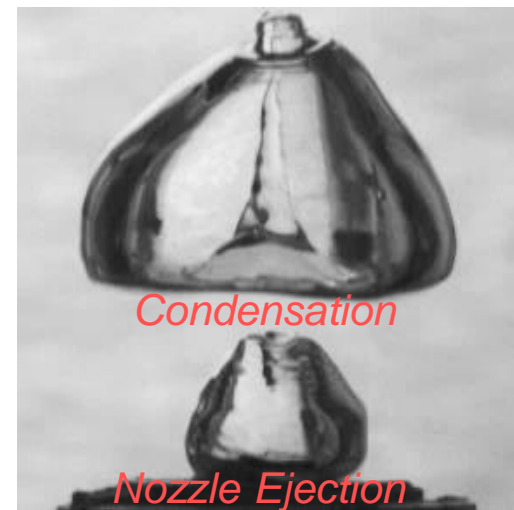
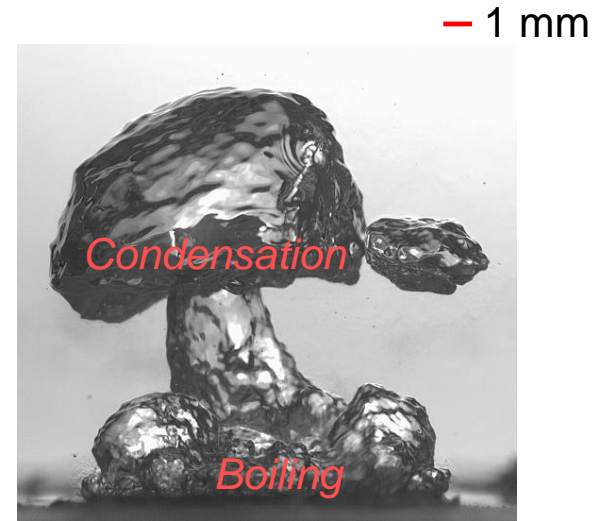


- Marginal increase in CHF (16%)
- Decrease in surface superheat of  $\sim 1$  °C
- Appearance of vapor is markedly different due to surface capillary waves
  - » Increased condensation has minimal effect on boiling process



# Acoustic Control of Vapor Condensation

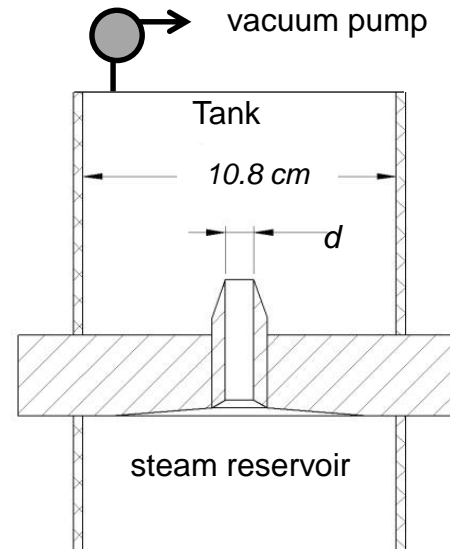
- Pool boiling and condensers both require enhanced condensation
  - » Pool boiling used in heat sink applications
    - Vapor boils and condenses in close proximity
  - » Condensers used in power cycles
    - Vapor is injected; boiling occurs in separate boiler component
    - Nozzle geometry interacts with vapor formation and acoustic enhancement
- Condensation is limited by interface area
  - » Thermal boundary layer surrounds vapor



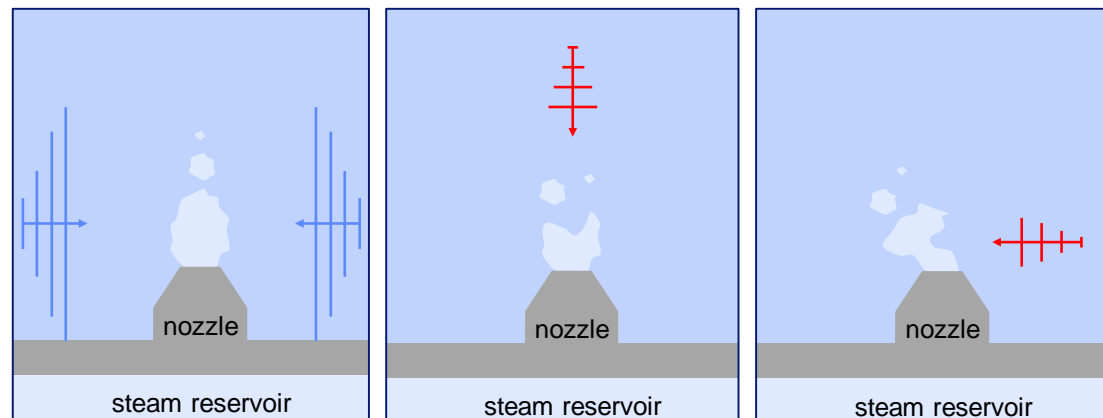
— 1 mm

# Acoustically Controlled Condensation Experimental Setup

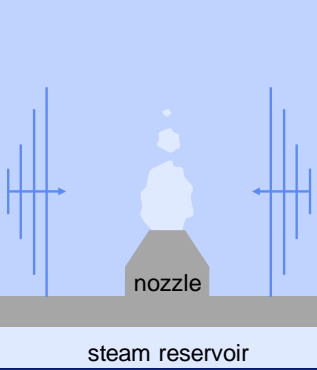
- Vacuum pump sets the ambient pressure in test cell
- Middle plate separates boiling from condensation
  - » Nozzle geometry can be varied
  - » Bulk temperature of upper tank controlled with coil heat exchanger (not shown)
  - » Immersion heater creates vapor in lower tank
- Acoustic actuators:
  - » 1 kHz, placed to sides of nozzle
  - » 1.7 MHz, oriented either above or to side of nozzle



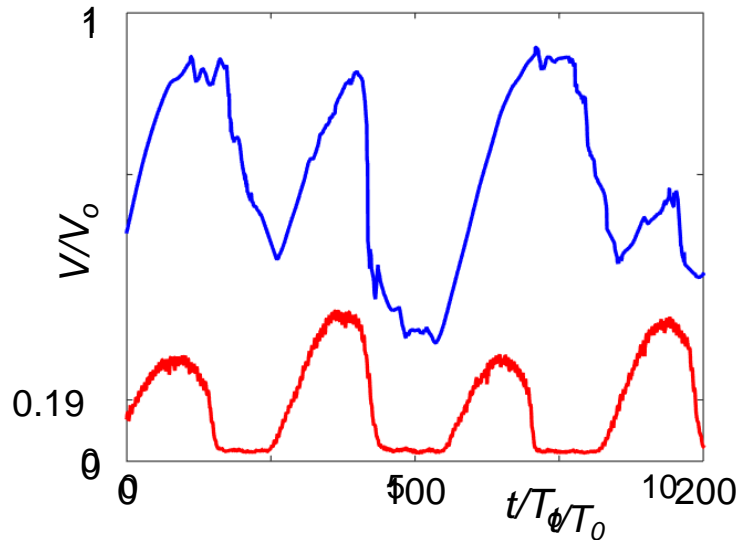
Distilled water  
0.15 – 1 atm



# Acoustically Enhanced Bubble Condensation Low Frequency (1 kHz)



Increased thermal interfacial mixing leads to rapid collapse.



$$A^* = \frac{\text{Vapor Area}}{\text{Average Baseline Vapor Area}}$$

$T_0$ : acoustic actuation period  $\approx 1$  msec

Base Flow



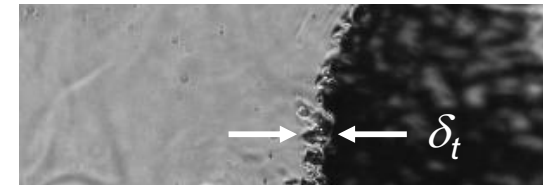
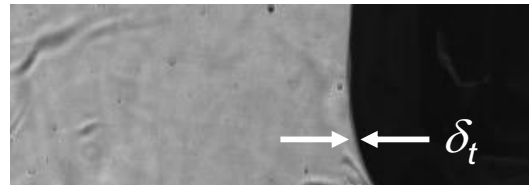
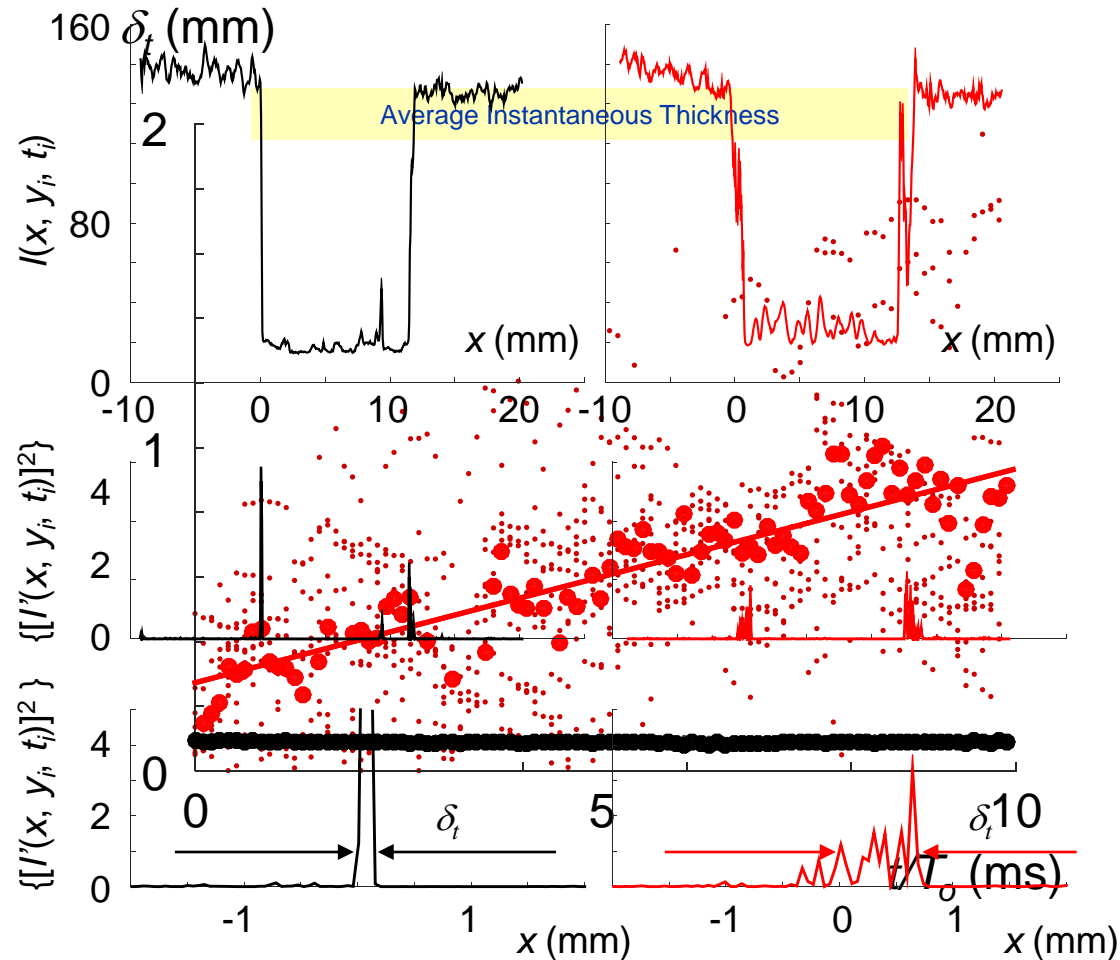
Actuated





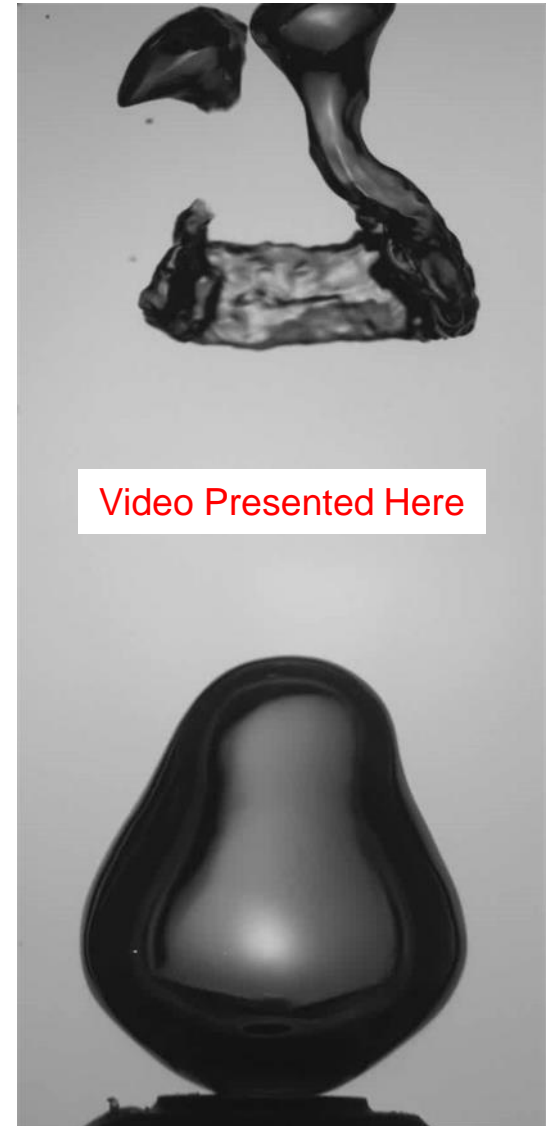
# Boundary Layer Growth - kHz Condensation

- Image processing of Schlieren images yields quantitative information on boundary layer growth
- Thermal boundary layer in baseline flow does not undergo appreciable growth
  - » Heat transfer occurs primarily through lower (and subsequently, inner) interface
- Acoustic actuation leads to nearly linear growth of boundary layer thickness
  - » No significant temporal dependence on acoustic actuation
- Thermal boundary layer in presence of acoustic actuation is on average 6.7 times thicker
  - » Up to 17 times thicker



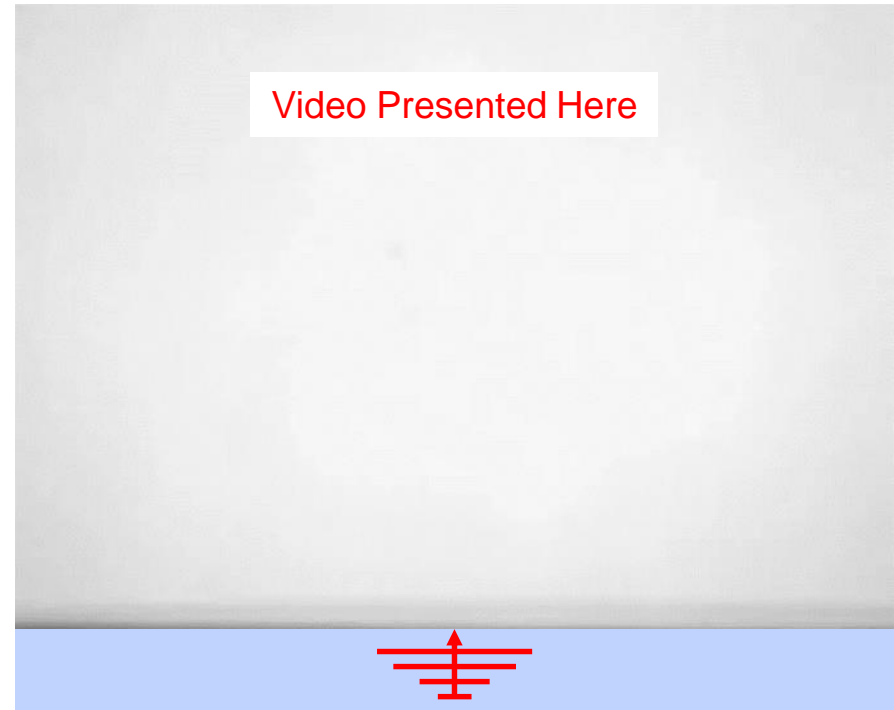
# Natural Deformation-Induced Vapor Collapse

- Surface tension pinch-off drives a liquid “spear” through the center of the vapor bubble to form a vapor torus that leads to rapid condensation.
- Schlieren imaging shows insignificant thermal gradients in fluid surrounding bubble.
  - » Inner “spear” enhances heat transfer
- This natural mechanism indicates that inducing such a liquid “spear” early in the bubble formation process can lead to accelerated condensation.



# Ultrasonic Liquid-Gas Interfacial Actuation

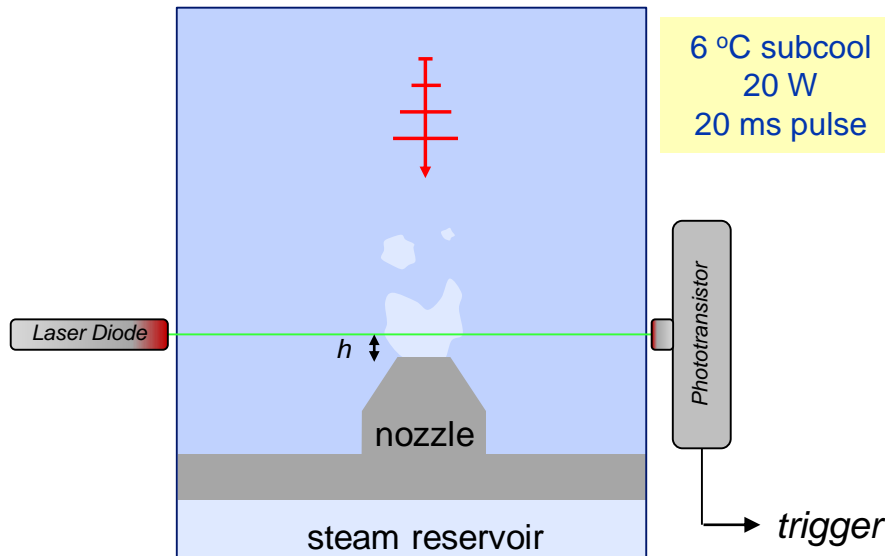
- $f = 1.7 \text{ MHz}$ 
  - ≈  $\lambda_{\text{acoust}} = 0.9 \text{ mm}$ ;  $D_{\text{res}} = 2 \text{ }\mu\text{m}$
  - ≈  $\lambda_{\text{capillary}} = O(\mu\text{m})$
  - » “Mist” droplets ejected, visible in video
- Cavitation and subsequent collapse generates additional droplets
  - » Larger-scale; not uniformly sized
- Acoustic impedance mismatch
  - »  $Z_{\text{vapor}}/Z_{\text{water}} = 1.8 \times 10^{-4}$
  - » Surface deforms from acoustic pressure
    - Deformed surface self-focuses acoustic intensity



1 cm

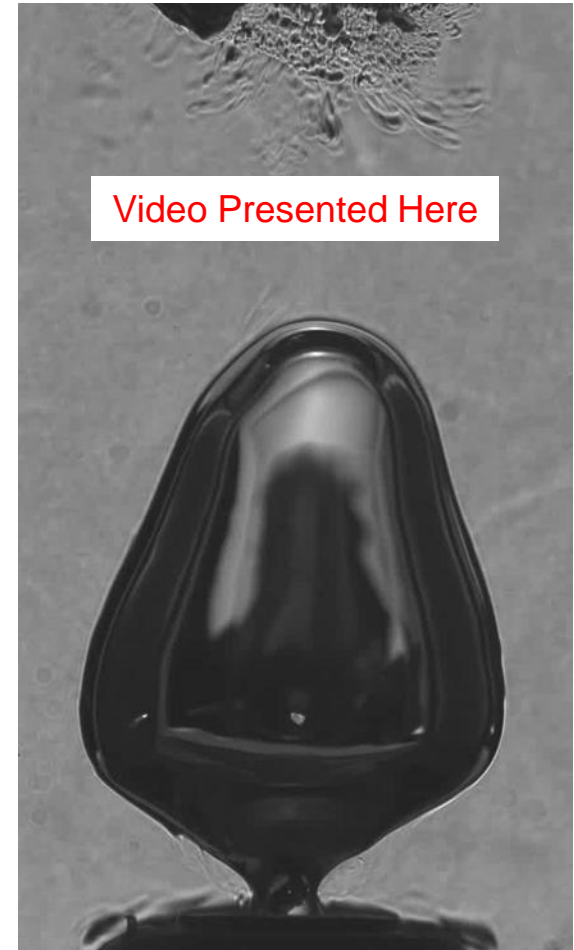
# Condensation Enhancement: Pulsed Ultrasound

Significant savings in actuation power



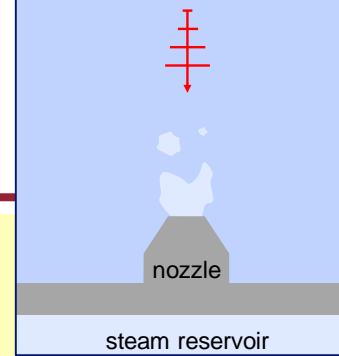
Schlieren Imaging

Video Presented Here

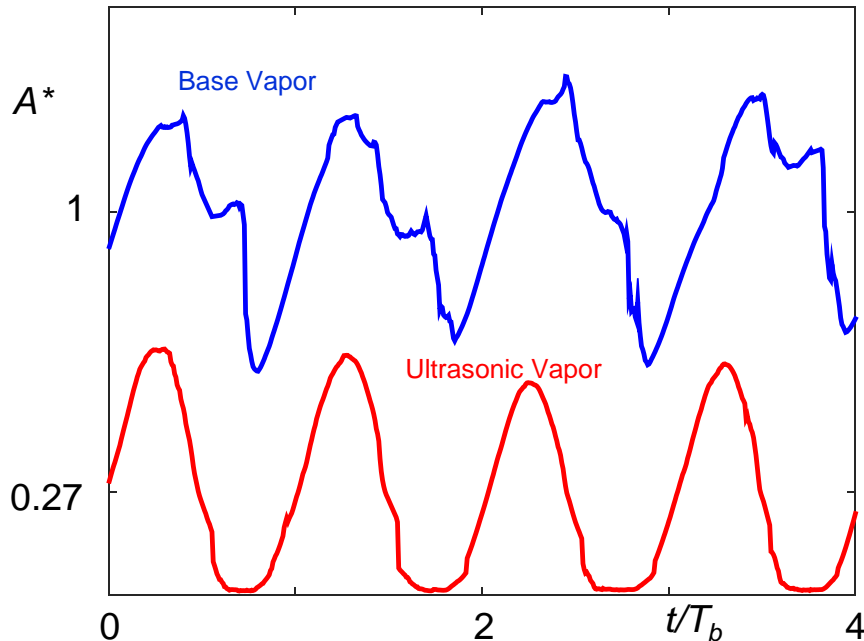


- Pulsed actuation.
  - » Saves power
  - » Minimizes interference with vapor ejection
  - » Vapor ejection pressure remains unchanged
- Pulse actuation is synchronized to “natural” bubble formation.
  - » Bubble phase reference is obtained using a trigger laser beam at given height above nozzle
  - » Actuation wavefronts are monitored using Schlieren imaging

# Axially-Aligned Pulsed Ultrasound Actuation



Triggering laser diode  
5 mm above nozzle  
 $Q = 225 \text{ W}$   
 $T_b = 50 \text{ ms}$   
Subcooling =  $25 \text{ }^\circ\text{C}$



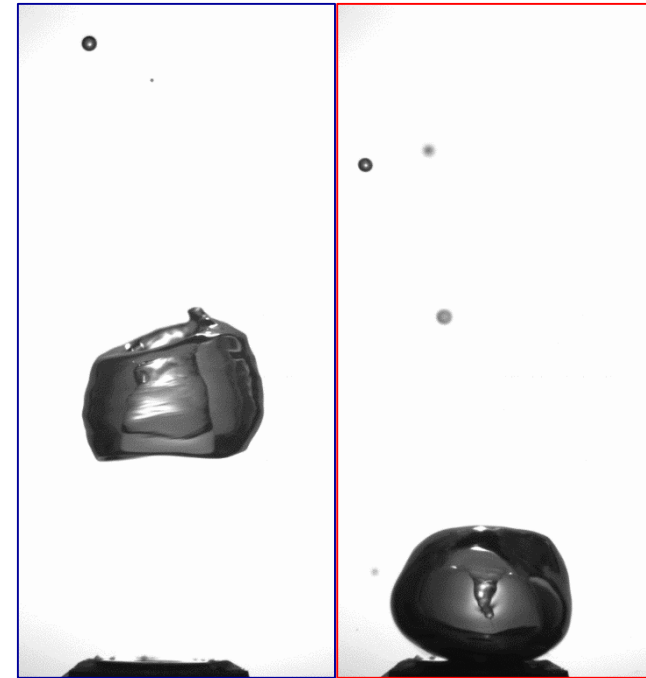
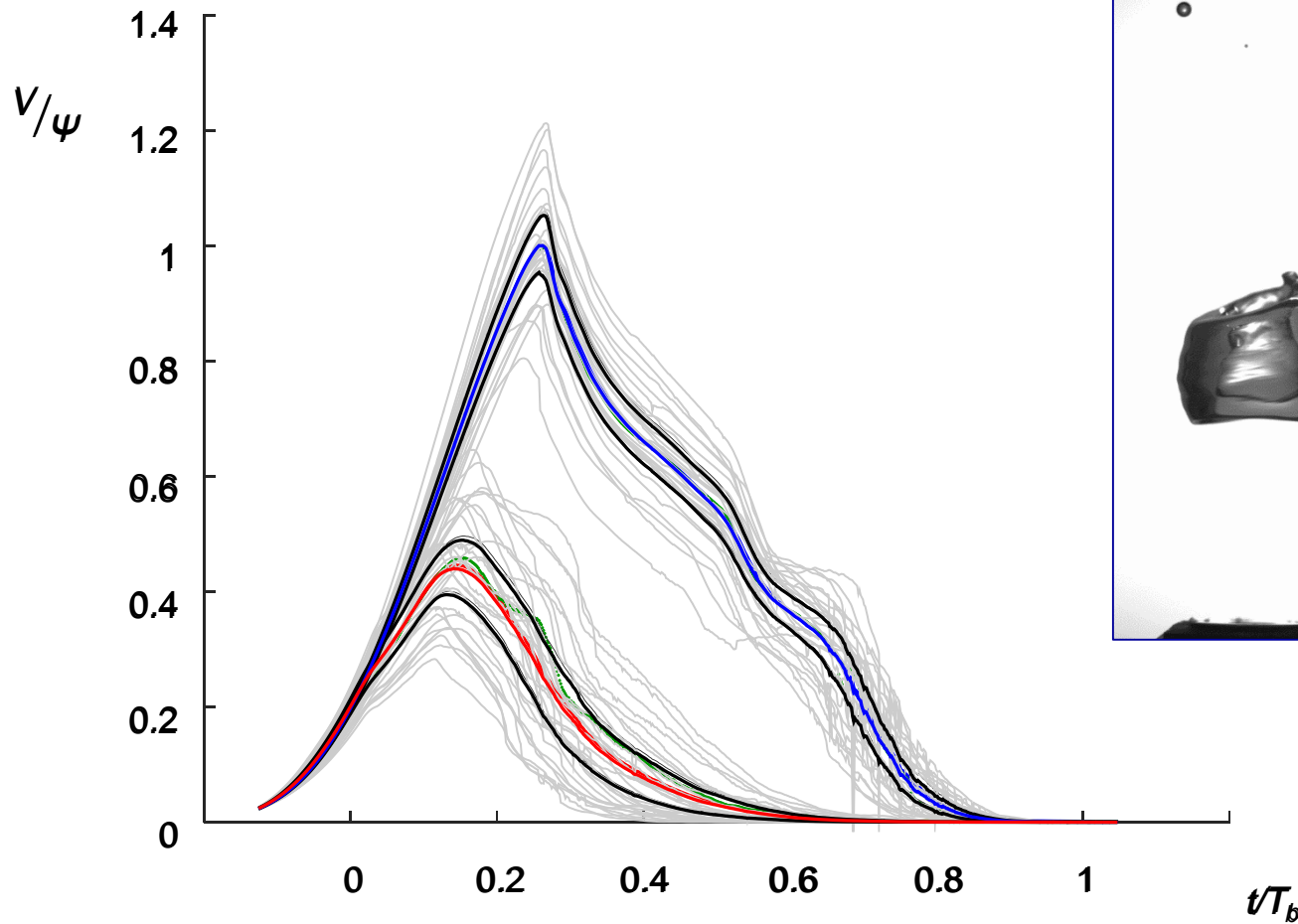
- High-speed video image processing yields an estimate of total vapor domain as function of time.
  - » Subcooling and heater dissipation are invariant, leading to the relation between vapor domain and heat transfer coefficient.

$$q_{base} = U_{base,eff} A_{base,eff} (T_{sat} - T_s) = U A_{act,eff} (T_{sat} - T_s) = q_{act}$$

$$\xrightarrow{\text{yields}} \frac{U_{act,eff}}{U_{base,eff}} = \frac{A_{base,eff}}{A_{act,eff}}$$

- Vapor domain reduced by up to 73% using 20 ms actuation pulses.
  - » HTC increased by 270%
- Actuation “regularizes” time-periodic bubble formation.
  - » The base flow a new bubble is ejected while the earlier bubble collapses
  - » In the presence of actuation, bubble collapse is completed prior to ejection of the subsequent bubble

# Bubble Volume Tracking

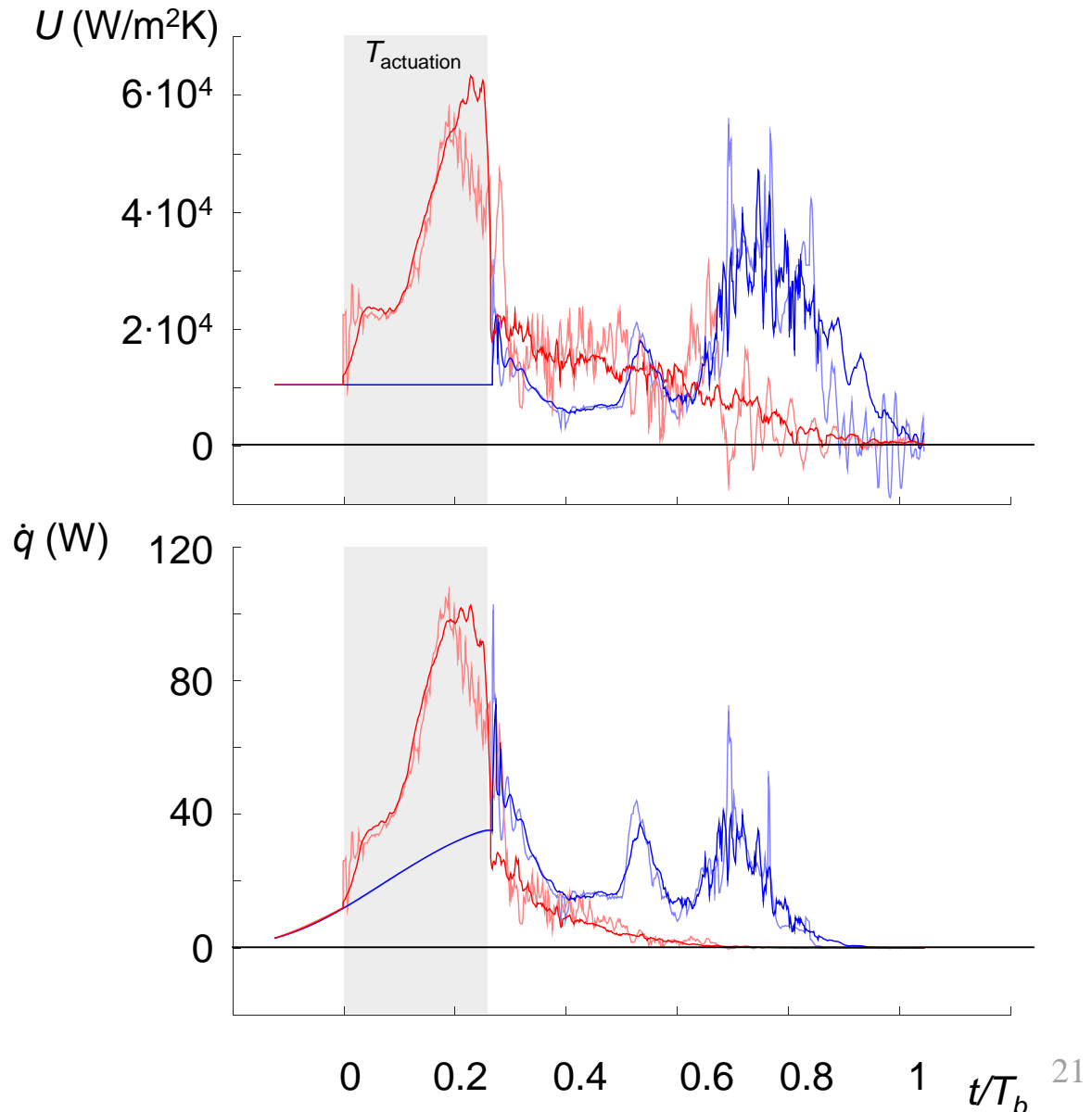


8 °C subcool  
20 W  
20 ms pulse  
 $T_b = 80$  ms  
 $\psi = 0.822$  cc

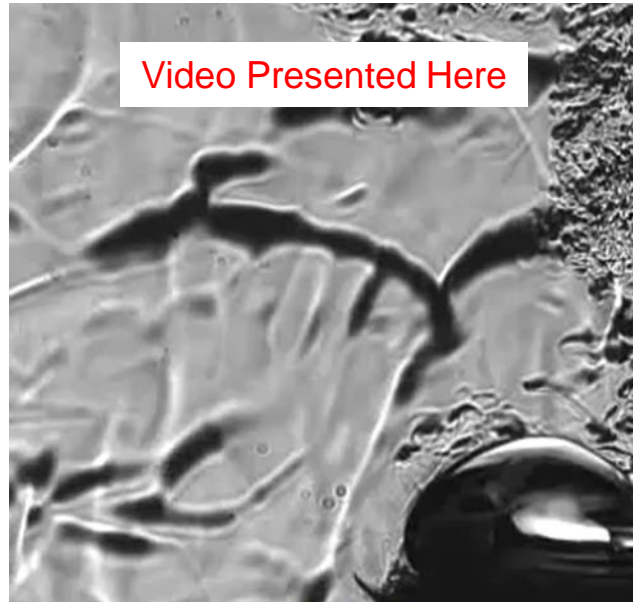
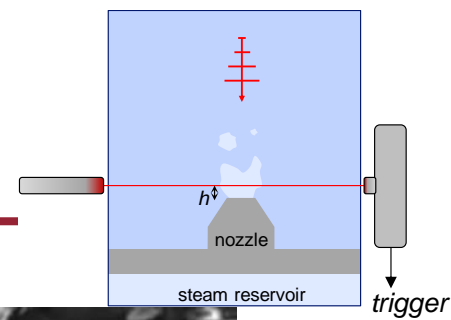


# Temporal Variation: Heat Transfer Coefficient and Heat Rate

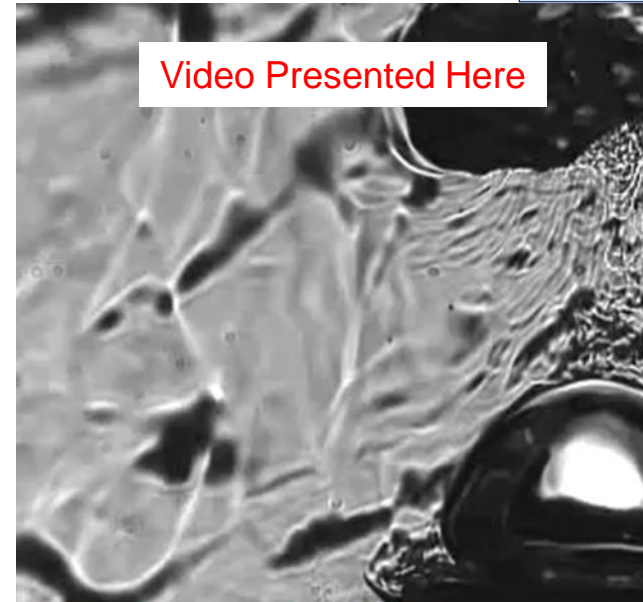
- Peak heat transfer coefficient occurs during toroidal breakup in the absence and presence of actuation.
  - » Acoustic actuation leads to near-immediate doubling of HTC
- Peak heat rate occurs during pinch-off, torus formation, and toroidal breakup
- Non-spherical effects
  - » Lower peaks and higher troughs



# Interfacial Disturbances by Secondary Droplet Ejection



Base Flow

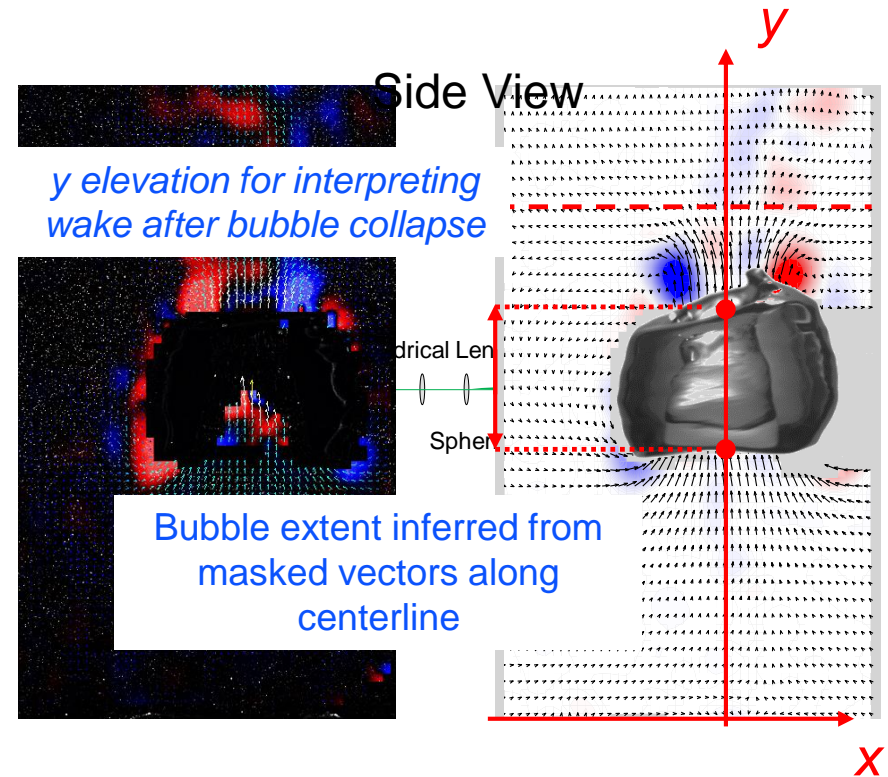
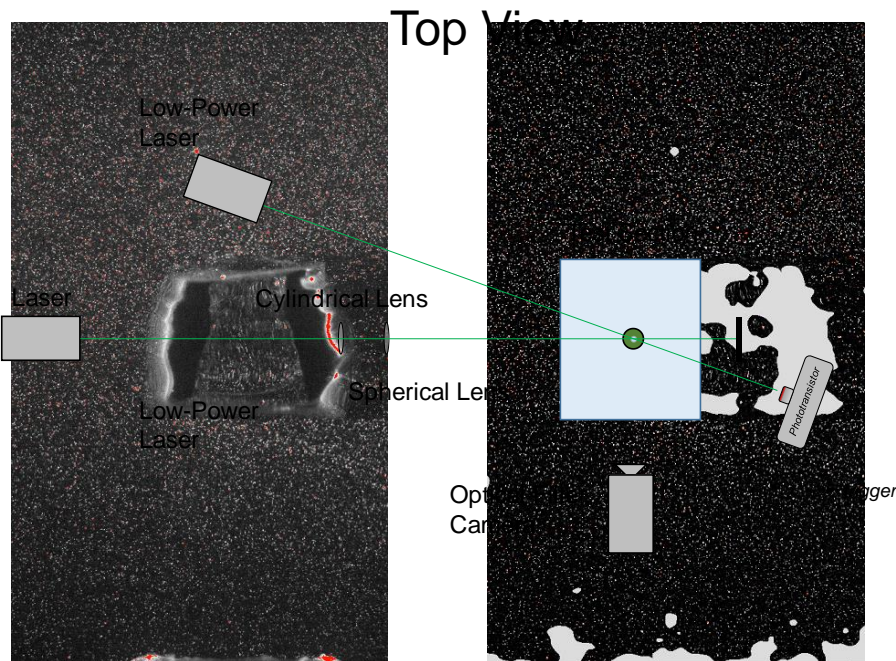


Pulsed Ultrasound Actuation

- High-resolution Schlieren imaging reveals formation of ultrasonically induced droplet ejection from spear.
- Required mass for complete phase change:  

$$m_{\text{droplets}} = E / (c_p \cdot \Delta T) = [(V_o / v_g) \cdot h_{fg}] / (c_p \cdot \Delta T)$$
- $m_{\text{droplets}}$  per pulse: 0.0207 gram/pulse.
  - » Can contribute up to 60% at low subcooling (8 °C), small bubbles or 45% at high subcooling (25 °C), large bubbles

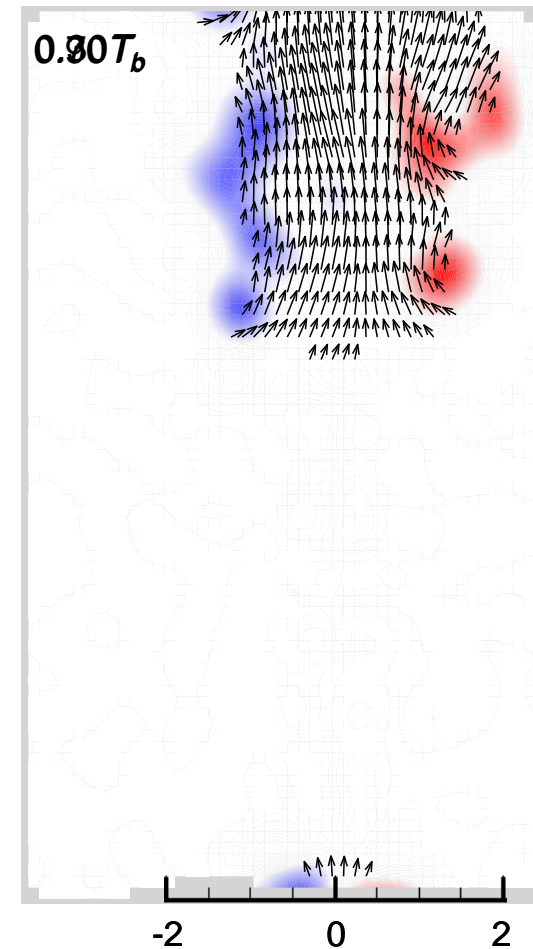
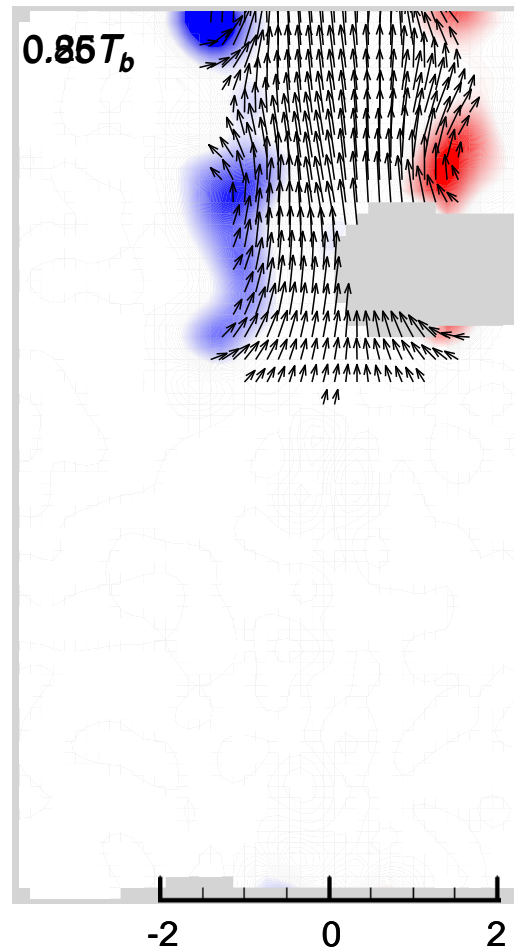
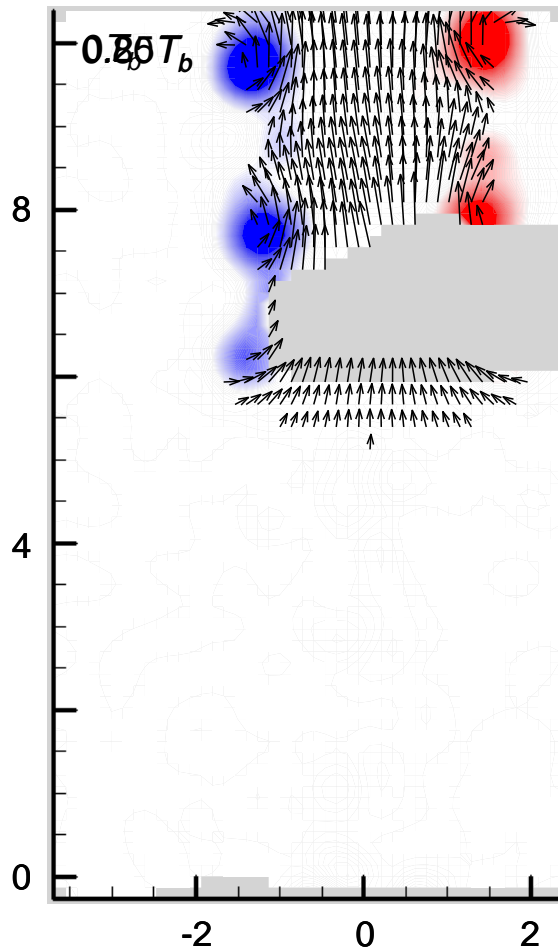
# Particle Image Velocimetry



- Fluorescent Particles and optical filter to reduce laser reflections
- Algorithmic masking to remove interface/ non-particle-laden flow
- Post processing: 10,000 fps flow fields temporally averaged over 0.5 ms (5 frames)
  - » Rightward of bubble is masked to remove interior and bubble shadow

# Naturally Condensing Vapor Bubbles

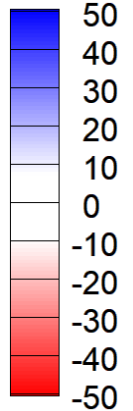
$y/d_o$



Plotting  
Threshold:  
 $0.55 V_t$

$\uparrow 1 V_t$

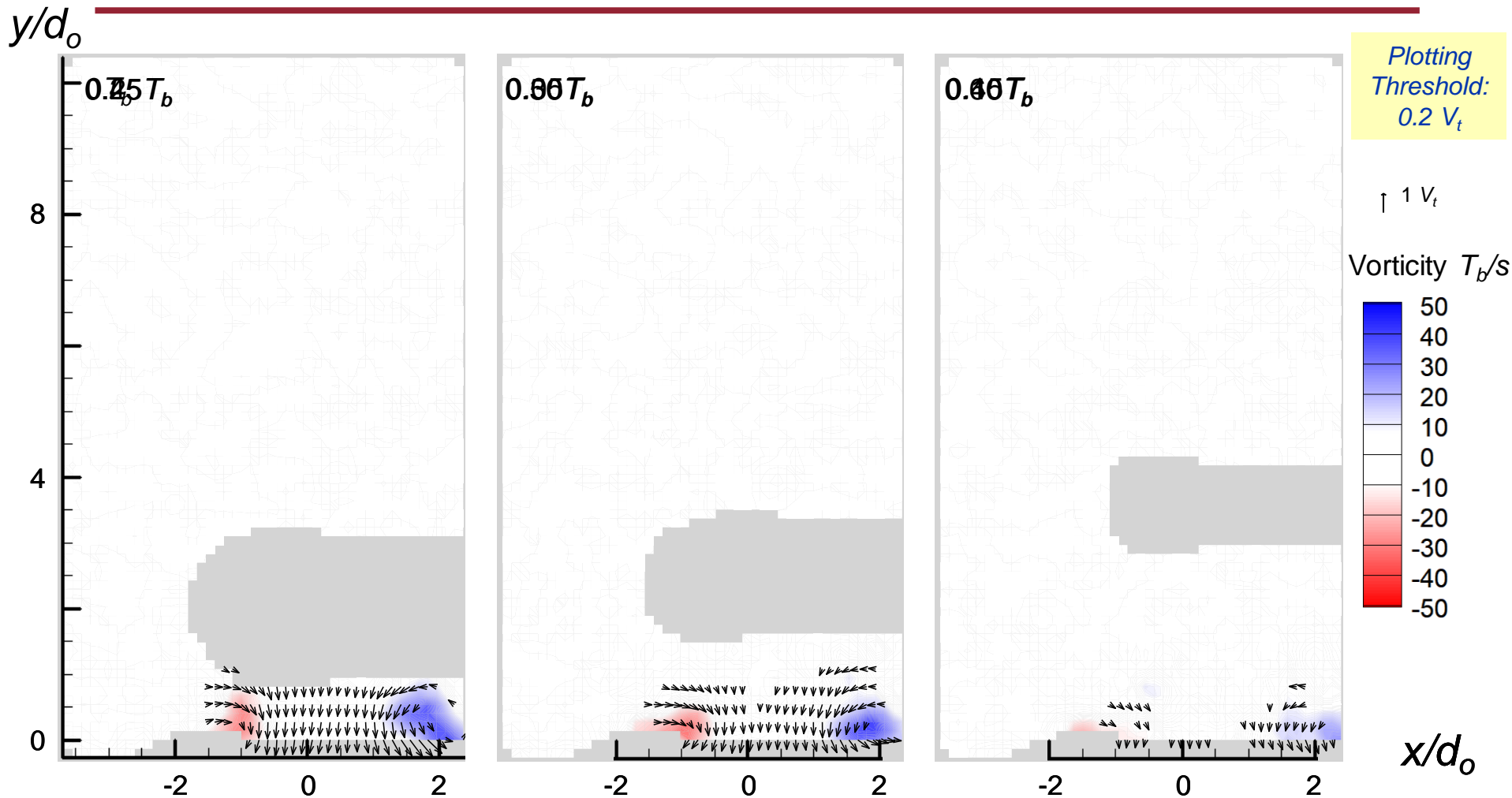
Vorticity  $T_b/s$



$x/d_o$



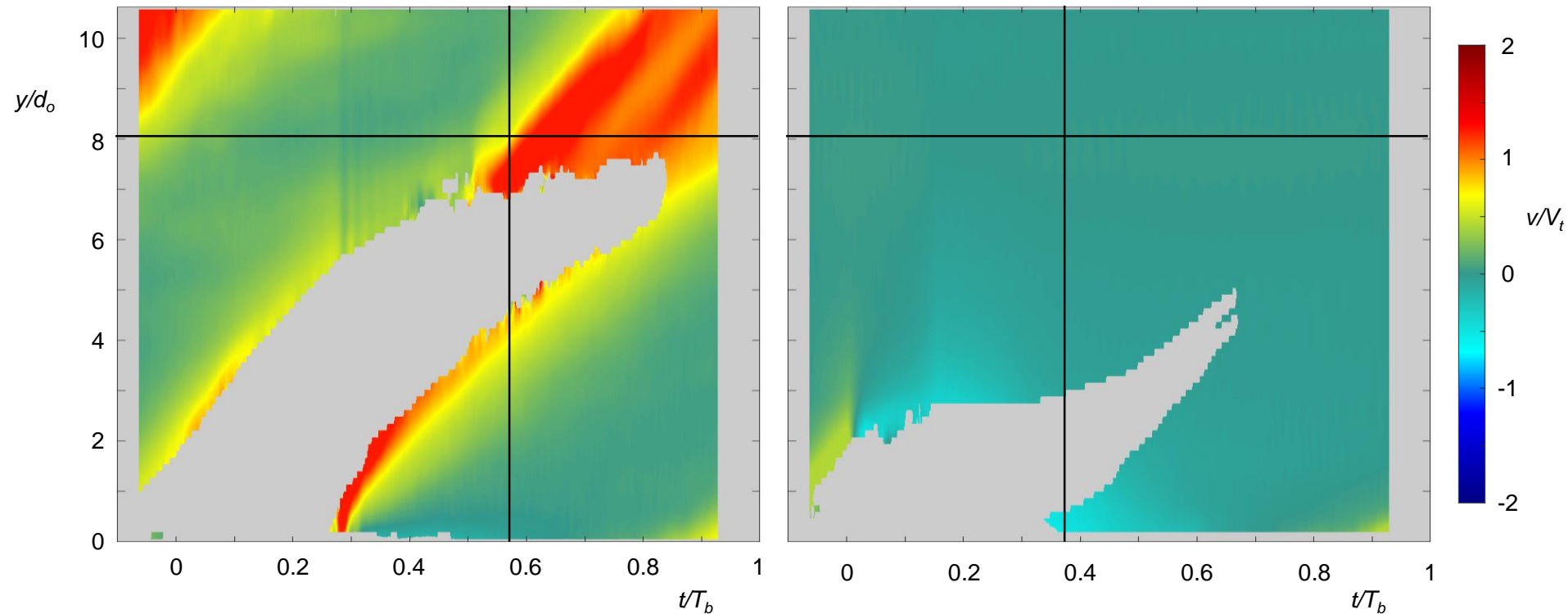
# Acoustically Actuated Vapor Bubbles



# Centerline Velocity

Base Flow

Actuated Flow

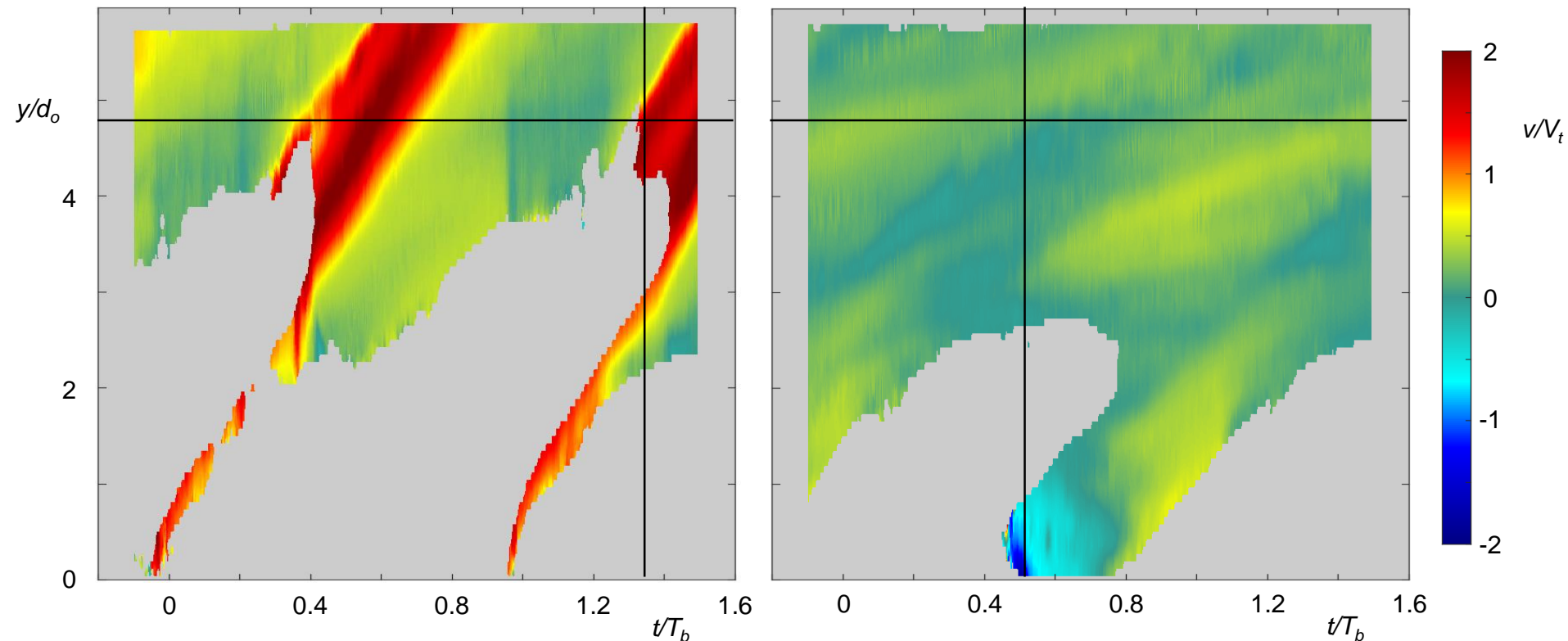




# High-Subcooling, High-Mass Flow Rate Vapor

Base Flow

Actuated Flow



# General Conclusions

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- Acoustic actuation is an effective method for controlling two-phase flows with heat transfer.
  - » Interfacial coupling varies with actuation wavelength
    - Low frequency,  $O(1 \text{ kHz})$ ; long wavelength = 1 m
    - High frequency,  $O(1 \text{ MHz})$ ; short wavelength =  $O(1 \text{ mm})$
  - » The acoustic coupling forces liquid-vapor interfacial motion that affects vapor formation, advection, and condensation.
  - » Strongly enhances pool boiling heat transfer.
  - » Accelerates direct-contact vapor condensation.

# Conclusions: Boiling

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- Ultrasonic actuation (short wavelength).
  - » Couples to vapor bubbles by a surface force.
  - » Vapor bubble nucleation, growth, and detachment are modified.
  - » CHF increases by 65%; surface temp. increases by 7 °C.
  - » Condensation increases above the boiling surface.
  - » Actuation may be turned on and off as needed without a drop in performance.
- Textured surfaces with ultrasonic actuation.
  - » Microchannels alone increase CHF to 350 W/cm<sup>2</sup>.
    - Ultrasound increases CHF to 460 W/cm<sup>2</sup>.
  - » Ultrasound *reduces* surface superheat by 7 °C (in contrast to smooth heater).

# Conclusions: Condensation

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- O(1 kHz) acoustic actuation (long wavelength).
  - » Interfacial Faraday waves increase condensation in the bulk liquid.
  - » Interface motion induces a temporally-growing thermal boundary layer.
  - » Condensation rate is increased both during growth and after advection, with increases of up to 425% in the time-averaged overall heat transfer coefficient.
  - » Importance of motion in inducing mixing implies effectiveness scales with surface displacement.
    - Lower frequencies (1 kHz or below).
    - Prior work used either extremely low (50 Hz) or high (20 kHz) frequencies, with smaller improvements in HTC.
- Ultrasonic acoustic actuation (short wavelength).
  - » Subcooled liquid jet protrudes into vapor bubble, significantly increasing vapor surface area and heat transfer coefficient.
  - » Formation of toroidal volume leads to rapid bubble collapse.
  - » Pulsed actuation causes up to a 73% reduction in vapor extent.